Authors' reply to referee comments RC1 of the paper tc-2023-148 entitled "Multiscale modeling of heat and mass transfer in dry snow: influence of the condensation coefficient and comparison with experiments" by Bouvet et al.

We thank very much Reviewer 1 for his fruitful comments. Please find below our point-by-point replies in blue color.

- 5 The manuscript reports on the multi-scale modeling of the heat and mass transfer in dry snow by using the homogenization technique to derive the macroscopic equations. The heat transfer is ruled by the conduction mechanism in ice and water vapor phases whereas the mass transfer of water vapor is described by the Fick's 2nd law. At the ice/fluid interface, the Hertz-Knudsen relation is used to describe the sublimation/deposition mechanism. For different order of magnitude of the sublimation/deposition rate, different cases (A, B1, B2 and C) are considered giving rise to different macroscopic models characterized by the
- 10 effective coefficients. The details of the homogenization procedure are given in the supplementary document while the main results of the macroscopic models are summarized in the manuscript. First, I verified the homogenization procedure in the "long" supplementary document for the cases A, B1, B2 and C. The notations are quite heavy with the superscript ? for each term and it can be simplified. In general, I agree with these results except for the case B2 (see my comments below). For high order of magnitude of the sublimation/deposition rate (or high value of α), this gives the same result obtained from the volume
- 15 averaging method reported in Moyne et al. (1988) for the heat and mass transfer with condensation/evaporation problem in porous media. The paper is interesting and well written. The development of the multiscale models is rigorous with a wellposed ε -models from the dimensional analysis. For this reason, I recommend the paper for publication after revision. Major comments:
 - 1. The authors should explicitly explain the choice of using the Hertz-Knudsen equation for describing the vapor flux at

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the solid/fluid interface. Instead of using an equilibrium condition at the solid/fluid interface as (the curvature effect is neglected)

$$k_i \nabla T_i \cdot \mathbf{n} - k_a \nabla T_a \cdot \mathbf{n} = \frac{L_{sg}}{\rho_i} D_v \nabla \rho_v \cdot \mathbf{n}$$
(1)
$$\rho_v = \rho_{vs} \quad \text{at } \Gamma_{fs},$$
(2)

the authors introduce Hertz-Knudsen law to take into account the non-equilibrium state for small value of α . It means that an "complementary resistance" is added at the solid/fluid interface. This point should be clearly discussed at the beginning. Moreover, maybe it should be better to define the latent heat of sublimation by $L = L_{sg}/\rho_i$ in J/kg.

In the present work, we have considered that the condensation-sublimation processes arising at the ice-air interface are driven by the Hertz-Knudsen equation. This latter equation, initially derived to describe the condensation-evaporation processes at a liquid-gas interface, is widely used in snow physics and is supported by several experimental evidences (e.g., Libbrecht, 2005; Kaempfer and Plapp, 2009; Furukawa, 2015; Libbrecht and Rickerby, 2013; Krol and Löwe, 2016). The Hertz-Knudsen equation is linearly dependent on the condensation coefficient α , which characterizes the probability (theoretically ranges from 0 to 1 for an infinite flat surface) that a water vapor molecule striking the ice surface is incorporated into it (see e.g., Libbrecht, 2005; Furukawa, 2015). As suggested by the reviewer, this coefficient α can be also seen as a "complementary resistance" at the solid /fluid interface. The above considerations were included in the revised version of the manuscript (line 118) to better explain the choice of the Hertz-Knudsen equation.

We agree with the suggestion of the reviewer that defining the latent heat of sublimation by $L_{sg}^{\rho} = L_{sg}/\rho_i$ in J/kg would simplify the expression thorough the paper. However, for the sake of consistency with our previous works (Bouvet et al., 2023; Calonne et al., 2014, 2015), we prefer to keep the same notation.

40 2. Dimensional analysis: the ratio of the heat conductivities of ice and air is

$$[K] = \frac{k_{ic}}{k_{ac}} = 96 \simeq \mathcal{O}\left(\varepsilon^{-1}\right) \tag{3}$$

However, the authors assume that [K] = O(1). This point needs to be clarified.

We agree with the reviewer that $[K] = O(\varepsilon^{-1})$ if we assume that $\varepsilon = 5 \times 10^{-3}$, i.e. $l \approx 5 \times 10^{-4}$ m and $L \approx 0.1$ m. If we assume that $[K] = O(\varepsilon^{-1})$, it is equivalent to neglect the effect of the thermal conductivity of the air on the effective thermal conductivity. In the analysis, we have kept [K] = O(1) for two reasons: (i) to keep the influence of the air on heat transfer for the case of extremely porous snow, and (ii) to ensure the continuity of the thermal conductivity at the boundary between the ice and the air phase. Moreover, let us remark that, in practice, ε may be of the order 10^{-4} (for small grains, $l \sim 0.1$ mm and a snowpack thickness L = 1 m), in that case [K] = O(1).

50 3. I don't agree with the result of the model B2. From Eqs. B2.22 and B2.23 together with the periodicity condition, we have

$$\int_{\Gamma} \left(\rho_v^{(1)} - \rho_{vs}^{(1)} \right) dS = 0 \tag{4}$$

where $\rho_v^{(1)}(x, y, t)$ is periodic function depending on x and y. This can not ensure that $\rho_v^{(1)} = \rho_{vs}^{(1)}$ on Γ is a unique solution. I suggest that the authors should find a solution for $\rho_v^{(1)} - \rho_{vs}^{(1)}$ by linearity as

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$$\rho_v^{(1)} - \rho_{vs}^{(1)} = \chi \cdot \nabla_x T^{(0)}$$
 (5)

combined with a solution for $\rho_{vs}^{(1)} = \gamma \mathbf{r}_a \cdot \nabla_x T^{(0)}$, so that from Eqs. B2.22 and B2.23, we can obtain a consistent closure problem with a coupled term at the solid/fluid interface.

We agree with this comment, and substantial modifications were made accordingly in the revised version of the manuscript. Taking into account the remarks of the reviewer, we have revised the derivation of the models (B2, C1). These modifications give rise to a new model called "C" in the revised version of the article. The model "C" ensures the continuity between the model B and D (the model D of the new version of the manuscript corresponds to the model C in the initial version) when $[W_R] = O(1)$, i.e $\varepsilon^{1/2} < [W_R] < \varepsilon^{-1/2}$ and thus when $\alpha_{\min} = (\varepsilon^{1/2} D_{vc}/(lw_{kc})) < \alpha < \alpha_{\max} = (\varepsilon^{-1/2} D_{vc}/(lw_{kc}))$. In dimensionless form, this model is written:

$$(\rho C)^{\text{eff}*} \frac{\partial T^{*(0)}}{\partial t^*} - \operatorname{div}_{x^*}(\mathbf{k}^{C*} \mathbf{grad}_{x^*} T^{*(0)}) = L_{sg}^* \dot{\phi}$$
(6)

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$$\phi \frac{\partial \rho_{vs}^{*(0)}}{\partial t} - \operatorname{div}_{x^*}(\mathbf{D}^{\mathrm{C*}}\mathbf{grad}_{x^*}\rho_{vs}^{*(0)}(T^{*(0)})) = \rho_i^* \dot{\phi}$$

$$\tag{7}$$

where $(\rho C)^{\text{eff}*}$ and $\mathbf{k}^{\text{C}*}$ are the dimensionless effective thermal capacity and the effective dimensionless thermal conductivity respectively, defined as:

$$(\rho C)^{\text{eff}*} = (1-\phi)\rho_i^* C_i^* + \phi \rho_a^* C_a^*$$
(8)

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$$\mathbf{k}^{\mathrm{C}*} = \frac{1}{|\Omega|} \left(\int_{\Omega_{\mathrm{a}}} k_a^* (\mathbf{grad}_{y^*} \mathbf{s}_a^* + \mathbf{I}) \mathrm{d}\Omega + \int_{\Omega_{\mathrm{i}}} k_i^* (\mathbf{grad}_{y^*} \mathbf{s}_i^* + \mathbf{I}) \mathrm{d}\Omega \right)$$
(9)

and where \mathbf{D}^{C*} is the dimensionless effective diffusion tensor defined as:

$$\mathbf{D}^{C*} = \frac{1}{|\Omega|} \int_{\Omega_a} D_v^* (\mathbf{grad}_{y^*} \ (\mathbf{d}^* + \mathbf{s}_a^*) + \mathbf{I}) \mathrm{d}\,\Omega$$
(10)

where $\mathbf{s}_i^*(\mathbf{y}^*)$, $\mathbf{s}_a^*(\mathbf{y}^*)$ and $\mathbf{d}^*(\mathbf{y}^*)$ are periodic vectors solution of the following coupled boundary value problem in a compact form:

$$\operatorname{div}_{y^*}(k_i^*(\operatorname{\mathbf{grad}}_{y^*}\mathbf{s}_i^* + \mathbf{I})) = 0 \quad \text{in } \Omega_i$$
(11)

$$\operatorname{div}_{y^*}(k_a^*(\operatorname{\mathbf{grad}}_{y^*}\mathbf{s}_a^*+\mathbf{I})) = 0 \quad \text{in } \Omega_a$$
(12)

$$\mathbf{s}_i^* = \mathbf{s}_a^* \quad \text{on } \Gamma \tag{13}$$

$$(k_i^*(\mathbf{grad}_{y^*}\mathbf{s}_i^* + \mathbf{I}) - k_a^*(\mathbf{grad}_{y^*}\mathbf{s}_a^* + \mathbf{I})) \cdot \mathbf{n}_i = \frac{L_{sg}^*}{\rho_i^*} \alpha^* w_k^* \gamma^*(T^{*(0)}) \mathbf{d}^* \quad \text{on } \Gamma$$
(14)

$$\operatorname{div}_{y^*}(D_v^*(\operatorname{\mathbf{grad}}_{y^*}(\mathbf{d}^* + \mathbf{s}_a^*) + \mathbf{I})) = 0 \quad \text{in } \Omega_a$$
(15)

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$$D_v^*(\mathbf{grad}_{y*}(\mathbf{d}^* + \mathbf{s}_a^*) + \mathbf{I}) \cdot \mathbf{n}_i = \alpha^* w_k^* \mathbf{d}^* \quad \text{on } \Gamma$$
(16)

with

$$\frac{1}{|\Omega|} \int_{\Omega} (\mathbf{s}_{\mathrm{a}}^* + \mathbf{s}_{\mathrm{i}}^*) \mathrm{d}\Omega = \mathbf{0}$$
(17)

$$\frac{1}{|\Omega|} \int_{\Gamma} \mathbf{d}^* \mathbf{d}\Gamma = \mathbf{0}$$
(18)

The vector \mathbf{s}_i^* , \mathbf{s}_a^* and \mathbf{d}^* depend on the value of α and of the temperature (notably through $\gamma^*(T^{*(0)})$). The evolution of the parameters \mathbf{k}^{C} and \mathbf{D}^{C} with respect to α is illustrated below in Figure 1 for the particular case of the simplified 2D geometry presented in the section 3.3 of the manuscript, assuming that k_i and k_a are constant. This new figure was also added in the new version of the manuscript (Figure 10). The following description of the figure was also included line 550: 'Figure 10 shows the evolution of the dimensionless diffusion coefficients D^{eff}/D_v , D^{C}/D_v and D^{D}/D_v and of the macroscopic thermal conductivities k^{eff} , k^{C} and k^{D} with respect to α and for two temperatures of 270K and 250K. As expected, only the parameters of the model C (D^{C}/D_v and k^{C}) vary with α and ensure a continuous transition between the parameters of the model A (D^{eff}/D_v and k^{eff}) and the ones of the model D (D^{D}/D_v and k^{D}). Fitting the numerical estimates, such transition can be described by a simple function:

$$\frac{D^{\mathrm{C}}(\alpha) - D^{\mathrm{eff}}}{D^{\mathrm{D}} - D^{\mathrm{eff}}} = \frac{k^{\mathrm{C}}(\alpha) - k^{\mathrm{eff}}}{k^{\mathrm{D}} - k^{\mathrm{eff}}} = \frac{\tilde{k}^{\mathrm{C}}(\alpha) - \tilde{k}^{\mathrm{B}}}{\tilde{k}^{\mathrm{D}} - \tilde{k}^{\mathrm{B}}} = \frac{A\alpha}{1 + A\alpha}$$

where A = 1200 is a constant.'

4. In my opinion, the effect of the sublimation/deposition needs to be better discussed in the macroscopic results in the Section 2.6. For example, for the case C, what I understand is that considering the sublimation/deposition at the solid/fluid

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Figure 1. Evolution of the dimensionless diffusion coefficients D^{eff}/D_v , D^{C}/D_v and D^{D}/D_v and of the macroscopic thermal conductivities k^{eff} , k^{C} and k^{D} with respect to α and for two temperatures (270K and 250K). The black lines represents the proposed function Eq. (89) to describe the parameters of the model C. Numerical estimates of the diffusion coefficient on 3D snow microstructures of different densities from Fourteau et al. (2021) are represented by the dot symbols.

interface refers to a classical heat conduction problem for ice and air without sublimation/deposition with a modified air conductivity being $k_a + k_{dif}$.

When α tends towards 1, i.e. $[W_R] > O(1)$, we have shown that $[H] = k_{dif_c}/k_{a_c}$ (see section 2.4) and consequently the microscopic problem becomes a classical heat conduction problem. Thus, in that case, the sublimation/deposition process induces at the first order an increase of the air conductivity through k_{dif} , which is proportional to the latent heat. This result is consistent with the results obtained from the volume averaging method reported in Moyne et al. (1988).

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5. I find that the discontinuity between the models B and C is quite surprising. Let consider only a heat conduction problem with a resistance at the solid/fluid interface as reported in Auriault and Ene (1994). All the one equation models can be deduced from one to other. The discontinuity appears when passing from two equations models to one equation model. However in this work, the one equations models are not continuous. By revisiting the model B2 (see my comment 3), can we obtain the continuity of the models?

Thanks to the remark of the reviewer (comment 3), a new model "C" has been derived, which ensures now the continuity between the models B and D, as presented in our reply of comment 3. This new model "C" was included in the revised version of the manuscript.

6. Page 17, line 410: it was concluded that if a temperature gradient is applied along e2, the model A (or B) will not predict any mass variation. In this direction, $D_{22}^{eff} = 0$ and at the steady state, we have $\rho_v^{(0)} = \rho_{vs}^{(0)} (T^{(0)})$ which varies according to the Clausius Clapeyron's law.

We wanted to point out that in that case there is no variation of porosity, i.e of the snow density. Indeed in the case of the model B, according to the equation (37), in steady state condition, we have $\dot{\phi} = 0$. (since $\mathbf{grad}\rho_{vs}^{(0)} = \gamma(T^{(0)})\mathbf{grad}T^{(0)}$ is along \mathbf{e}_2 only). This part has been changed accordingly in the revised version of the manuscript.

7. Page 21, line 470: for the water vapor boundary conditions at the top and bottom, why the Robin boundary condition is imposed instead of using the zero-flux as applied for the macro-scale simulations?

We agree with this remark. Simulations at the micro-scale were thus performed again and a zero-flux was applied. The obtained results do not differ significantly from the previous applied conditions, as shown by the figures below (Fig. 2 and 3). These updated figures were included in the revised version of the manuscript (Figure 12 and 13).

8. Comparison between DNS and macroscopic simulations: In Figs. 11(a) and (b) for ΔT , we observe clearly that by increasing α , the DNS result tends to the one of model C and for higher value of α ($\alpha > 1$), we may have a good agreement between the DNS and the model C as expected. However, in Fig. 11(f), why the result of the DNS for $\alpha \rightarrow 1$ does not tend to the case C for $\dot{\Phi}$? Moreover, as the model C is independent on α , I suggest that to compare with the simulation of the model C, for the mass transfer problem at the pore scale, the equilibrium should be used at the solid/fluid interface $\rho_v = \rho_{vs}$ at Γ , instead of using the Robin condition involving the parameter α .

The figures 2 and 3 presented here were updated in the revised version of the manuscript and correspond to Figures 12 and 13 (figures 11 and 12 in the initial manuscript). They take into account the new results from the micro-scale simulations (see previous comment) as well as the predictions of the new model C. These figures show that a better agreement between the model predictions and the fine scale simulations occurs when α tends towards 1. However, we can still observe some differences for α -values in the range $10^{-5} - 1$, which may be due to the inaccuracy of the mass balance equation. A boundary layer must be introduced to better predict sublimation/deposition in the vicinity of the bottom and top boundaries.

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9. It is observed that the model B and C can not predict correctly the behavior of sublimation/deposition in the vicinity of the boundary, in comparing with the DNS. In my opinion, it refers to a boundary layer problem (several works in the literature try to fix this problem encountered in simulation of homogenized models).

We agree with the reviewer that a boundary layer can be introduced, as in the case of heterogeneous reactions in porous
 media, at the bottom and the top of the snowpack to better predict sublimation/deposition in the vicinity of these boundaries. This problem will be addressed in future works.

- 10. The terminology "boundary condition" used to describe the solid/fluid interface condition is not correct. Please modify this sentence to "interface condition".
- 155 In the revised version of the manuscript, the terminology "boundary condition" has been replaced by "interface condition" as suggested by the reviewer.



Figure 2. Vertical profiles of ΔT , $\rho - \rho_{vs}(T)$, and $\dot{\phi}$ from the pore scale simulations (dots) and from the macroscopic model A (grey lines), B (orange lines), C (magenta lines) and D (blue lines), considering a temperature gradient of 100 and 500 K m⁻¹ and for different values of α . ΔT represents the deviation of the temperature profile from a linear temperature profile.



Figure 3. Temperature and water vapor density in the middle of the snow layer as a function of α , obtained from the pore-scale simulations (dots) and from the macroscopic model A (grey lines), B (orange lines), C (magenta lines) and D (blue lines), at 100 and 500 K m⁻¹. The models are only shown for the α -values within their domain of validity. Values of saturation water vapor density ρ_{vs} from the pore-scale simulations and from the model A are also presented.

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